

Engineering the surface of perovskite $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ for catalytic activity of CO oxidation†

Cite this: *Chem. Commun.*, 2014, 50, 9200

Received 2nd January 2014,
Accepted 25th June 2014

DOI: 10.1039/c4cc00023d

www.rsc.org/chemcomm

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A simple treatment of $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ with diluted HNO_3 creates more B-sites (rich) on the terminated perovskite surface and improves its catalytic activity toward CO oxidation, and the perovskite catalyst possesses a higher ratio of $\text{Mn}^{4+}/\text{Mn}^{3+}$ and thus enhances the O_2 adsorption capability, favourable for CO oxidation and catalytic activity.

Design of efficient catalysts providing better-controlled active sites for fundamental studies of heterogeneous catalysis and developing novel industrial catalysts is the ultimate goal of research on heterogeneous catalysis.¹ Generally, the size, shape, composition, and interface/surface engineering in catalytic materials are the key parameters that are usually considered in synthesis to exhibit the rule of catalyst dependence.^{2,3} Since heterogeneous catalysis usually occurs on solid surfaces providing the appropriate electronic and/or geometric environment, design of active sites on the surface requires precise control on the atomic scale.^{1,4} As a promising candidate for the replacement of noble metals, which are commonly expensive and exhibit limited stability, perovskite oxides (especially $\text{La}(\text{Sr})\text{MnO}_3$ and $\text{La}(\text{Sr})\text{CoO}_3$) are emerging as automotive exhaust catalysts.^{5,6} However, J. T. S. Irvine⁷ reported that native perovskite surfaces are preferentially A-site (rich), not catalytically active sites,⁸ terminated to the detriment of the B sites, which results in the true catalytic properties of many perovskites based on ideal bulk-like terminated surfaces which might have been underestimated due to their fundamental flaw. There is still a lack of fundamental understanding of

the perovskite surface catalytic mechanism at the atomic/molecular level. To overcome these disadvantages, a clean procedure to create more B-site (rich) terminated perovskite surfaces and related catalytic property investigations are greatly in need.

Acid/base treatment of catalysts was regarded as one of the most widely accepted method to improve specific performance in porous TiO_2 ,⁹ zeolites,¹⁰ layered perovskites¹¹ and carbon materials.¹² Treatment with H_2O_2 and NH_4OH for modification of surface electronic and magnetic properties in perovskite films was also reported.¹³ However, to date no work on the wet-etching treatment of perovskite catalysts has been reported for activating the perovskite.

Herein, we developed a method to modulate the perovskite surface of $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ samples, *e.g.*, treatment of dilute HNO_3 solutions with controlled time followed by the evaluation of the corresponding catalytic activity for CO oxidation. Our finding demonstrates that the simple surface treatment shows the importance of B-site (rich) terminated perovskite surface control in harnessing the true catalytic potential of perovskite oxides and opens up strategies for the development of the activity for other perovskite transition-metal oxides.

The raw sample was synthesized *via* a hydrothermal route adapted from a previous report with minor modification.^{14,15} The details of sample preparation and the acid activation process are given in the ESI.† Upon increasing treatment time, the crystal structure remains the same as the raw sample, which can be indexed to a primitive cubic unit cell (in Fig. 1 space group $Pm3m$, $a = 3.841 \text{ \AA}$). Inductively coupled plasma elemental analysis of the raw sample confirmed the energy dispersive spectrometry (EDS) result (inset of Fig. 3a) and indicated that its bulk composition is $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$. Usually, the yielded raw $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ particles are La, Sr-enriched on the surface and this phenomenon of A-enriched in other perovskite systems often appears.^{7,16–18} The surface composition changes from La, Sr-rich to Mn-rich by the modification of simple treatment by dilute HNO_3 solutions. Surface composition was evaluated by X-ray photoemission spectroscopy (XPS) which is a surface sensitive technique for probing the surface composition and the electronic structure.

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† Electronic supplementary information (ESI) available: Sample preparation, characterization details, the catalytic performance evaluation process, and N_2 adsorption-desorption, the valence state of Mn and O 1s spectra, and Arrhenius activation energy data. See DOI: 10.1039/c4cc00023d

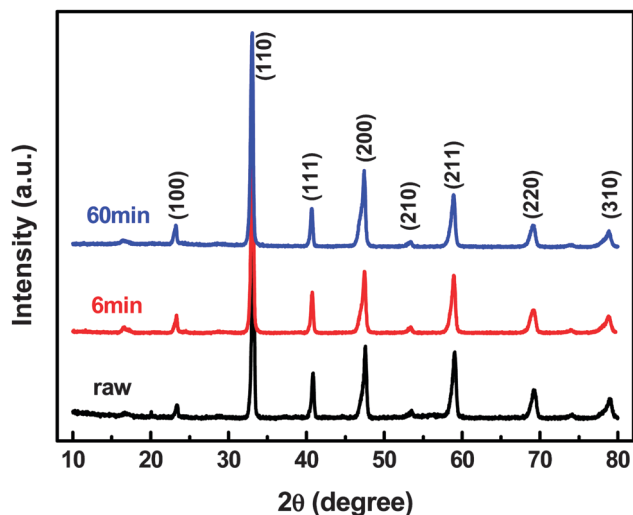


Fig. 1 X-ray diffraction patterns of $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ for the raw sample without treatment (#1), and samples treated with dilute nitric acid solution for 6 min (#2) and 60 min (#3).

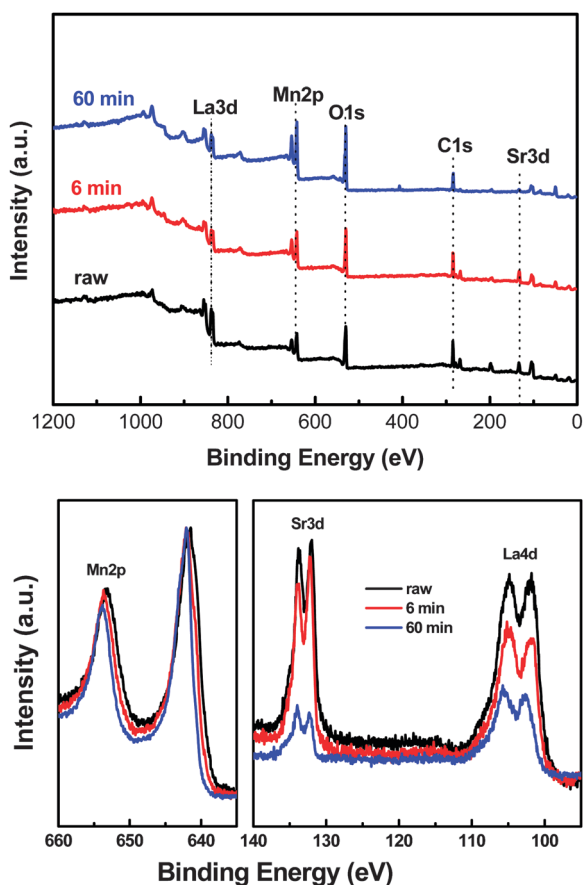


Fig. 2 XPS survey and Mn 2p, Sr 3d and La 4d spectra for the three samples #1, #2 and #3. (intensity of Sr 3d and La 4d were adjusted to the normalized Mn 2p.)

According to XPS quantitative analysis, the surface composition of the raw synthesized $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ is 39.0 atom% of Mn/(La + Sr + Mn) (Fig. 2), which indicates La, Sr-enrichment

on surfaces, in terms of ideal 50.0 atom% in EDS data. Change of La, Sr and Mn atomic ratios can be easily observed from the intensity variation in XPS survey spectra and detailed narrow scan core-level spectra of normalized Mn 2p and related La 4d and Sr 3d electrons. XPS quantitative results indicated that the surface has 46.8 and 67.5 atom% Mn for samples of 6 min and 60 min treatment. In contrast, the corresponding results of surface composition measurements by EDS show that the bulk Mn/(La + Sr + Mn) molar ratios (inset of Fig. 3) were 51.2%, 56.3% and 64.5% for sample #1, #2 and #3, respectively. These results indicated that the A-site atoms were successfully removed by wet-etching treatment, while EDS results also exhibited a quite smaller decrease of A site atoms compared to XPS results. It is obvious that La, Sr or Mn enrichment of $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ particles was controlled from the surface to bulk process by selective wet-etching treatment time with a dilute acid at room temperature.

The scanning electronic microscope images revealed morphological evolution in an acidic environment, which improves the surface region from smooth in the ground raw material surface to a bit rough and fully ruffled surface, showing the possible reorganization of the surface structure (Fig. 3). The reason for selective removal of A-site atoms is the longer distance of La–O and Sr–O bonds than Mn–O bonds and the relatively high surface energy of the A–O bond. The surface electronic structure after treatment was improved, and the content of Mn^{3+} decreased and Mn^{4+} increased on the surface of Mn-rich particles. The ratios of $\text{Mn}^{4+}/(\text{Mn}^{3+} + \text{Mn}^{4+})$ are 40.2%, 62.8%, and 63.7% for samples #1, #2 and #3, respectively, as shown in Fig. S3 (ESI[†]). The additional Mn^{4+} promoted the formation of the surface oxygen vacancies. The production of Mn^{4+} at relatively high temperatures is important for the improvement of CO oxidation.^{19,20}

The catalytic CO oxidation over the as-obtained samples was evaluated in a $\text{CO-O}_2\text{-N}_2$ stream. As shown in Fig. 4, for the conversion of CO into CO_2 , T_{10} (the temperature of the conversion 10%) for sample #1, #2, #3 are 245, 169 and 158 °C and T_{50} (the half conversion temperature) are 340, 245 and 230 °C, respectively. To illustrate the relationship between enhanced catalytic behavior and the surface electronic structure, we schematically proposed the surface composition change, which indicates the elemental compositions, terminated layers on surfaces, and the corresponding surface evolution (Fig. 4). This means that the treated samples exhibited a much higher activity, which might be attributed to the presence of more active sites for creating a B-site (rich) terminated perovskite surface.

To further investigate the origin of different catalytic activity behaviors, temperature programmed reduction (TPR) of H_2 was tested to understand the relative reducibility closely related to its catalytic performance (Fig. S1, ESI[†]). For the raw samples (#1), the peak in the range of 700–800 °C most likely corresponded to the reduction of the remaining Mn^{3+} to Mn^{2+} , meanwhile, the peak at about 507 °C can be attributed to the reduction of Mn^{4+} to Mn^{3+} . The peak shifted to lower temperatures, which may result from a single-electron reduction of Mn^{3+} located in a coordination-unsaturated microenvironment.¹⁹ For samples

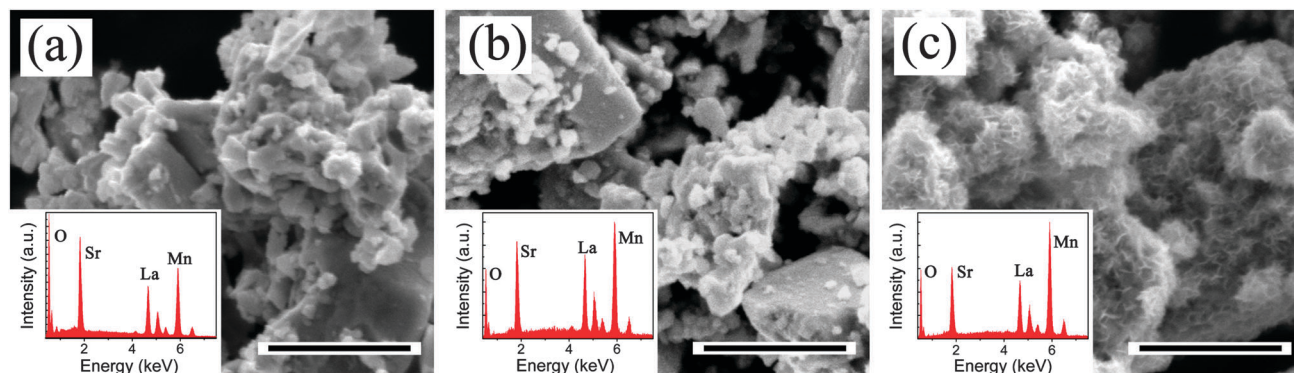


Fig. 3 SEM and EDS (inset) of $\text{La}_{0.5}\text{Sr}_{0.5}\text{MnO}_3$ (a) without treatment (1#), treated for (b) 6 min (2#) and (c) 60 min (3#). All scale bars are 1 μm .

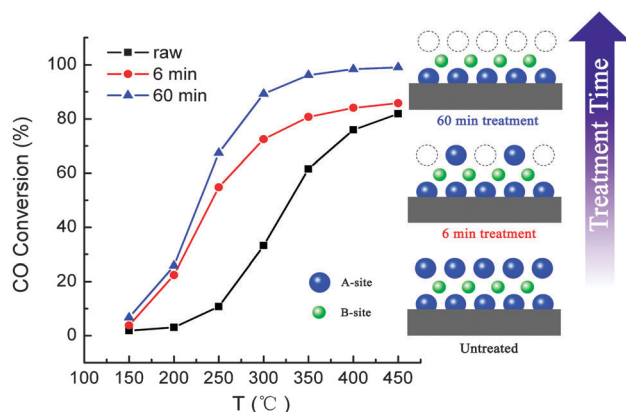


Fig. 4 Activity profiles of CO oxidation over the samples without treatment (raw), and treated with dilute nitric acid solution for 6 min and 60 min.

treated with dilute nitric acid solution for 6 (#2) and 60 min (#3), this situation may be favorable for the reduction of Mn^{4+} to Mn^{3+} at lower temperature as a result of the surface electronic structure change on the surface of Mn-rich particles. The peak at about 282 °C can be assigned to removal of nonstoichiometric excess oxygen accommodated within the lattice.¹⁵ It is obvious that the position shifted to lower temperatures for the treated samples, indicating the better reducibility. The TPR results suggest²¹ that high reducibility was achieved after the treatment with acid in this work, as it has been generally accepted that good redox property leads to excellent catalytic reactivity.²²

O 1s XPS was measured to investigate the oxygen species on the surface or lattice of catalysts. Free oxygen vacancy was produced for whole reactivity,²³ which can serve as active sites and can increase the oxygen exchange rate, favoring the interaction with CO. The corresponding concentrations of O_{ad} (adsorbed oxygen species)/ $\text{O}_{\text{lattice}}$ (lattice oxygen species) were obviously elevated (Fig. S3, ESI[†]), which was in good accordance with the observed catalytic activities and H_2 -TPR results.

In this work the method of acid treatment created B-site (rich) terminated perovskite surfaces to overcome their fundamental flaw for catalytic activity, meanwhile, leading to an

increased surface area (Fig. S2, ESI[†]). In order to eliminate the surface area effect, the apparent activation energy (E_a) of CO oxidation was calibrated (as shown in Fig. S4, ESI[†]). By comparing the E_a values of catalysts, one can evaluate their catalytic performance. The lower the E_a value is, the easier is the complete oxidation of CO.²⁴ The results clearly revealed that CO oxidation over three samples exhibits a surface-dependent catalytic activity similar to high-index planes dependence in some binary oxide systems (e.g. Co_3O_4 (ref. 25) and Cu_2O ²⁶), which are supposed to provide more active sites in either environments. However, the facets control for ternary perovskite oxides is much more difficult.²⁷ Therefore, this method applied here may give an alternative choice for enhancing surface dependent catalytic activities.

In summary, we have developed a reliable and ready method to create a B-site (rich) terminated perovskite surface for controllable selective wet-etching of perovskite-type oxides. Our wet-etching method can be applied to other perovskite-type oxides. We thus provide the fundamental engineering on metal oxide surfaces, which if properly controlled, can lead to radical enhancement of the catalytic activity.

This work was supported by the National Natural Science Foundation of China (Grants 90922034, 21131002, and 21201075) and Specialized Research Fund for the Doctoral Program of Higher Education (SRFDP Grant 20110061130005), and Natural Science Foundation of Jilin Province (Grants 20140520080JH).

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